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1 **The role of riboflavin in decolourisation of Congo red and bioelectricity production using**
2 ***Shewanella oneidensis*-MR1 under MFC and non-MFC conditions**

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7
8 **Abstract:**

9 Dissimilatory metal reducing bacteria can exchange electrons extracellularly and hold great
10 promise for their use in simultaneous wastewater treatment and electricity production. This study
11 investigated the role of riboflavin, an electron carrier, in the decolourisation of Congo red in
12 microbial fuel cells (MFCs) using *Shewanella oneidensis* MR-1 as a model organism. The
13 contribution of the membrane-bound protein MtrC to the decolourisation process was also
14 investigated. Within the range of riboflavin concentrations tested, 20 μM was found to be the
15 best with >95% of the dye (initial concentration 200 mg/L) decolourised in MFCs within 50
16 hours compared to 90% in the case where no riboflavin was added. The corresponding maximum
17 power density was 45 mW/m². There was no significant difference in the overall decolourisation
18 efficiencies of *Shewanella oneidensis* MR-1 ΔMtrC mutants compared to the wild type. However,
19 in terms of power production the mutant produced more power (P_{max} 76 mW/m²) compared to
20 the wild type (P_{max} 46 mW/m²) which was attributed to higher levels of riboflavin secreted in
21 solution. Decolourisation efficiencies in non-MFC systems (anaerobic bottles) were similar to
22 those under MFC systems indicating that electricity generation in MFCs does not impair dye

23 decolourisation efficiencies. The results suggest that riboflavin enhances both decolourisation of
24 dyes and simultaneous electricity production in MFCs.

25 **Key words: Electron shuttling, MtrC, *Shewanella*, dye decolourisation, energy production,**
26 **riboflavin**

27

28 **Introduction**

29 Azo dyes have been one of many synthetic dyes used in the textile industry. To this day, more
30 azo dyes are synthesized, not only for colouring purposes but also for biological-medical
31 imaging and other optical applications (Mohammadi et al., 2015). Research focusing on azo
32 decolourisation has always been in demand, focusing on novel ways to degrade this dye, the
33 danger always lying in the azo group ($-N=N-$). Methods may depend on physicochemical
34 removal such as adsorption on magnetic biocomposites (Sivashankar et al., 2015) or could rely
35 on biological removal depending on enzyme induction such as peroxidases, azo reductases etc.
36 Biological removal is considered more favourable for complete degradation of azo compounds
37 (Imran et al., 2016).

38 Biologically, the azo bond is thought to be cleaved under anaerobic conditions leading to
39 decolourisation but the mechanism is not clear. Since azo dyes are large and usually charged,
40 they are likely to be reduced extracellularly. It has been suggested that the decolourisation
41 process is a fortuitous one where azo dyes might act as an electron acceptor supplied by carriers
42 of the electron transport chain. There are also suggestions that decolourisation is due to non-
43 specific extracellular reactions occurring between reduced compounds of anaerobic metabolism
44 e.g. sulphides and the azo dyes. Others suggest that anaerobic reductive cleavage of the azo bond

45 is aided by azoreductases, the electron shuttling being aided by soluble redox mediators e.g.
46 flavins (Fernando 2014; Saratale et al., 2011)

47 Rau *et al.*, 2002 observed enhanced anaerobic reduction of azo dyes using *Escherichia coli* in
48 presence of quinoid redox mediators e.g. Anthraquinone -2-sulphonate and lawsone and
49 attributed this to induction of azoreductases. High concentrations though of lawsone (> 200 μM)
50 did not increase reduction rate possibly due to toxicity.

51 The use of microbial fuel cells (MFCs) has been considered a promising technology for both
52 decolourisation of azo dyes and electricity production (Hou et al., 2011, Pandey et al., 2016).
53 MFCs utilise electrochemically active bacteria to catalyse an oxidation reaction at the anode.
54 Electrons generated are channelled via an external circuit to a cathode electrode where they
55 recombine with protons and a terminal electron acceptor e.g. oxygen. The extracellular reduction
56 of azo moieties in the anode chamber is likely to occur using electrons coming from a co-
57 substrate e.g. glucose. Furthermore, the ability of MFCs to use oxygen or ferricyanide indirectly
58 as the terminal electron acceptor also confers MFCs an additional advantage over conventional
59 anaerobic systems in terms of faster microbial metabolic rates and growth rates that could
60 potentially be beneficial in achieving faster azo dye degradation kinetics in MFC anodes.

61 Different bacteria have the ability to degrade azo dyes, among which are those belonging to
62 family *Shewanellaceae* which is considered a model bacteria for studying electron transfer
63 (Carmona-Martinez et al., 2011). The electron transport process in *Shewanella* is thought to be
64 through one of two mechanisms: direct electron transfer which depends on the direct contact and
65 facilitated electron transfer which usually takes place via electron shuttles or mediators (Chen et
66 al., 2013). Direct electron transfer from the cytoplasm to an electron acceptor (e.g. azo dye) is

67 thought to be aided by a number of multi-heme cytochromes (CymA, MtrA, MtrB, MtrC,
68 OmcA) that span the inner membrane, periplasm and outer membrane. Electron shuttles are low
69 molecular weight organic molecules that are chemically stable, can easily diffuse into the
70 medium to pass on the electron to external electron acceptors and thus catalyse the
71 reduction/oxidation reactions (Velasquez-Orta et al., 2010). Some studies have suggested that
72 75% of the total electron transfer in *Shewanella* is due to shuttling by Flavin-based redox
73 mediators (Kotloski and Gralnick, 2013) leaving 25% for direct electron transfer.

74 There are different applications for electron shuttling in biotechnology, those include azo dye
75 reduction, enhancing electricity production in MFCs as well as halogenated organic compound
76 degradation. The electron shuttling molecules are usually derivatives of the following
77 compounds: Cobalamin, Phenazine, Naphthoquinone, Anthraquinone and Viologen (Watanaeb
78 et al., 2009)

79 One of the electron shuttle compounds is riboflavin, which is secreted by *Shewanella oneidensis*
80 MR-1 and is confirmed as an electron shuttle compound (Marsili et al., 2008). Flavins in general
81 play different roles for *Shewanella*; they were reported to be released to act, not only as growth
82 accelerators but also as electron shuttles during Fe (III) oxides reduction (von Canstein et al.,
83 2008). Riboflavin is a commonly known redox mediator (Hsueh et al., 2014) and its presence in
84 *Shewanella* biofilm was correlated to its electron transfer ability (Marsili et al., 2008).

85 It would be expected that supplementation of *Shewanella oneidensis* cells in MFCs with
86 Riboflavin would aid decolourisation. However, the situation in an MFC anode chamber may be
87 complicated by the presence of an anode which can also accept electrons depending on its redox
88 potential relative to that of the dye / electron donor. Co-substrate conversion in an MFC is

89 however, expected to be higher than in typical anaerobic systems as oxygen (or ferricyanide) is
90 used indirectly (in the cathode) as a terminal electron acceptor. It would also be expected that a
91 Δ MtrC mutant of *Shewanella oneidensis* would not decolourise azo dyes to the same extent as
92 the wild type strain because the direct electron transfer mechanism would not be in operation.

93 The aim of the present work was to assess the role of riboflavin in azo dye decolourisation as the
94 main dominant form of electron shuttling in *Shewanella oneidensis* MR-1 and to determine
95 whether the decolourisation process is competitive with electricity production. The contribution
96 of the MtrC cytochrome in the decolourisation process was also investigated.

97 **Material and Methods**

98 **Chemicals used**

99 Congo red (C.I Direct red 28), riboflavin and chemicals used for GC (purity \geq 96%) were
100 purchased from Sigma Aldrich, UK. For the chemical oxygen demand (COD) test, Ficodox
101 PlusTM mixed reagent was purchased from Fisher Scientific UK.

102 **Microorganisms and media used**

103 Microbial cultures used in this study were *Shewanella oneidensis* MR-1 (ATCC 700550) and
104 *Shewanella oneidensis* MR-1 Δ mtrC; the latter was kindly provided by Marcus Edwards, School
105 of Biological Sciences, University of East Anglia.

106 A loopful of strain seed was pre-cultured in 50 ml of LB media (Sigma Aldrich) overnight at 37
107 °C and 150 rpm. Then 20% (v/v) of the pre-cultured broth was inoculated into an MFC system
108 for cell propagation to stimulate dye decolourisation and/or bioelectricity generation.

109 Congo red decolourisation (50, 100, 200 and 400 mg/l), riboflavin addition (10, 20, 30, 40 μ M),
110 use of 10 mM of different inhibitors (sodium nitrate, copper sulphate, sodium azide and ferrous
111 sulphate) and cell entrapment in alginate beads were all performed in 20 ml bottles containing 5
112 ml LB media. Cultures were incubated at 30 °C overnight after purging with nitrogen gas for 10
113 minutes through 0.22 μ m pore size diameter filter. The used inoculum was 20% v/v.

114 **OD and Riboflavin concentration measurement**

115 The bacterial growth was monitored by measuring OD at 600 nm. Riboflavin concentration was
116 performed according to Xu et al., (2015) by measuring the absorbance at 444 nm

117 **Decolourisation in MFC systems**

118 MFC systems were H-type two chambered system with two identical Duran bottles held together
119 with external metal clamps. The electrodes were made of carbon fibre and were cut to 4 cm x 4
120 cm. The anode and the cathode compartments were separated with a cation-exchange membrane
121 CMI-7000 (Membranes International USA). The anaerobic anode compartment contained 200
122 ml working volume was purged with nitrogen gas for 10 minutes through 0.22 μ m pore size
123 diameter filter prior to inoculation, the media used was MSM prepared according to Fernando et
124 al., 2012, which contained the following (g/L): NH_4Cl 0.46, KCl 0.225, $\text{MgSO}_4 \cdot 7\text{H}_2\text{O}$ 0.117,
125 NaH_2PO_4 2.5, Na_2HPO_4 4.11, $(\text{NH}_4)_2\text{SO}_4$ 0.225, a vitamin mixture and trace mineral solution
126 was added (1%), 500 mg/L casein hydrolysate and 2.2 g/L sodium pyruvate were also added.
127 Air- saturated cathode contained 200 ml working volume of 0.1 M potassium ferricyanide in 50
128 mM sodium phosphate buffer (pH 7). MFC systems were incubated at 30 °C in a Stuart 160
129 Incubator (Fisher Scientific UK). Congo red (200 mg/l) was added to the anodic chamber for all
130 experiments, riboflavin concentrations used for the first experiment were in the following

131 concentrations: 10, 20 and 40 μM . *Shewanella oneidensis* MR-1 was used to inoculate the first
132 experiment. As for the second experiment, 4 MFC bottles were used, the first was inoculated
133 with *Shewanella oneidensis* MR-1, the second contained *Shewanella oneidensis* MR-1 and 40
134 μM riboflavin, the third was inoculated with *Shewanella oneidensis* MR-1 ΔmtrC and the fourth
135 (control) *Shewanella oneidensis* MR-1 and contained no dye. External resistance for all
136 experiments was 1000 Ω .

137 **Electrochemical measurements**

138 Voltage output data was collected using a Picolog ADC-24 (Pico Technology, UK) online data
139 logging system. Polarization tests were done by connecting different values of external
140 resistances once voltage had stabilized.

141 **COD tests**

142 The chemical oxygen demand removal was determined using the closed reflux titrimetric method
143 as described by Westwood (2007). COD was calculated as follows:

$$144 \text{ COD (mg/l)} = (V_b - V_s) * \text{DF} * \text{M} * 3200$$

145 Where V_b was the ferrous ammonium sulphate titrant of the blank, V_s was the ferrous
146 ammonium sulphate titrant of the sample, DF was the dilution factor, M was the molarity of the
147 ferrous ammonium sulphate titrant.

148 The percentage of COD removal was calculated as follows:

$$149 \text{ COD removal (\%)} = [\text{COD}_I - \text{COD}_T / \text{COD}_I] * 100$$

150 where COD_I and COD_T were the initial and final calculated COD values, respectively.

151 **Detection of by-products using Gas Chromatography**

152 To detect the by-products remaining at the end of the MFC operation, samples were withdrawn
153 from each system centrifuged at 14000 rpm for 15 min, filtered and placed in a 2 ml glass vial
154 tube for metabolite detection using a Varian 3900 GC system. The mobile phase consisted of a
155 carrier gas (helium) with a flow rate of 2 mL/min; the column was a 30 mm length x 0.320 mm
156 diameter x 0.50 µm film- HP INNOWax (Agilent J&W GC columns), injector temperature was
157 260°C. The oven was initially set at 35 °C for 5 min and then ramped up to 170 °C for the
158 subsequent 10 minutes. Detector temperature was 250 °C. The presence of degradation
159 metabolites ethanol, acetic acid and butyric acid was detected using the retention time of the
160 respective standard compounds.

161

162 **Decolourisation and UV-visible scans**

163 Decolourisation of Congo red dye was calculated as follows:

164
$$\text{Dye decolourisation (\%)} = (A_I - A_F) / A_I \times 100$$

165 where A_I is the absorbance of the dye at zero time, A_F is the absorbance of the dye at the end of
166 the operation process. The absorption maxima of Congo Red was 497 nm. UV-Visible scans for
167 the samples before and after decolourisation were performed using Perkin-Elmer Lambda-35
168 UV-Visible spectrophotometer; scans were performed within a range from 280-700 nm. Data
169 was collected using Perkin-Elmer UV Winlab 6.0.4.

170

171 **Toxicity assay**

172 The confocal microscope was used to study the impact of using riboflavin to enhance the
173 degradation of Congo red. A VL-17A cell line was used (HepG2 cells), About 250 µl was added
174 to wells in a 6 well plate. DMEM media with 10% FCS (3 ml) was added to each well and
175 incubated at 37°C overnight. The media was removed and replaced with 100 µl of the following
176 samples: 1) dye before decolourisation, 2) dye after decolourisation, and 3) positive control cells.
177 Samples were left to incubate overnight, after which, 300 µl of freshly prepared Calcein
178 fluorescent dye dissolved in DMSO (excitation and emission wavelength of 495/515 nm,
179 respectively) was added and the plate was left to incubate in darkness for another 45 min at 37°C.
180 Samples were then studied using confocal scanning laser microscope (CSML). Images were
181 acquired by sequential sequencing using Leica TCS SP2 confocal system (Leica Microsystems,
182 Milton Keynes, UK) and a X63 ceramic dipping objective at 1024x1024 format and scanning
183 speed of 400 Hz with a line average of 2.

184 Statistical analysis

185 All experimental data indicated on the graphs and table are the means of duplicate experiments
186 unless otherwise stated and the error bars in the graphs represent the standard deviation of the
187 mean (SD). Statistical analysis of data was conducted by one way analysis of variance
188 (ANOVA) using Microsoft Excel statistics package.

189 Results

190 Effect of riboflavin concentration on decolourisation and current production

191 Different amounts of riboflavin were added to *Shewanella oneidensis* MR-1 culture
192 supplemented with 200 mg/l Congo red in anaerobic serum bottles. The relationship between
193 decolourization and growth with the different concentrations is illustrated in Figure 1. The figure

194 shows that both decolourisation of Congo red dye increased with the increase in riboflavin
195 concentration; there were no changes in the decolourisation for concentrations above 40 μM . On
196 the other hand, the addition of riboflavin enhanced the growth profile. As the concentration of
197 riboflavin increased, the OD of bacterial growth showed an increase as well.

198 Fig. 2a represents the variation of current production with time in response to the addition of
199 different riboflavin concentrations. The Figure shows that the maximal current was produced
200 when 20 μM riboflavin was added to the MFC culture. The decrease in voltage in Figure 2a
201 when 20 μM Riboflavin was supplemented could be due to depletion of easy to use substrate
202 (sodium pyruvate) with the microorganisms starting to use fermentation end products e.g.
203 butyrate. The addition of 40 μM riboflavin resulted in less current production (perhaps due to
204 toxicity of riboflavin an high concentrations) and the minimal current production resulted after
205 adding 10 μM riboflavin to the MFC culture, which was less than that obtained for control (no
206 riboflavin). The same result was obtained for both the voltage and power density curves (Fig
207 2b&2c), where the addition of 20 μM riboflavin resulted in the highest voltage (510 mV) and
208 power density (45 mW/m^2).

209

210 **Deducing the pathway for electron transfer for decolourisation**

211 To investigate the mechanism by which *Shewanella oneidensis* MR-1 cells transfer electrons,
212 different approaches were tested and decolourisation was calculated. Fig 3 shows that
213 decolourisation increased from 81% for control (freely suspended cells, no riboflavin or
214 inhibitor) to 96.7% when riboflavin was added to the media. On the other hand, decolourisation
215 decreased when sodium nitrate (46.8%), copper sulphate (43.7%), sodium azide (52%), ferrous

216 sulphate (60.8%) and when cells were entrapped in sodium alginate beads (32%). Entrapment
217 was used to preclude direct contact between the bacteria and the azo dye in the media.

218 **The role of MtrC in decolourisation and current production**

219 To determine the role of MtrC, an MtrC knock out strain was used to compare its performance to
220 that for *Shewanella oneidensis* MR-1 wild type in the presence and absence of riboflavin. The
221 results shown in Figure 4a represent the decolourisation profile over 72 h. The figure clearly
222 shows that the rate of decolourisation increased gradually in the first 24 h, after which there was
223 a steady state that was maintained. Supplementation of the cultures with riboflavin gave a
224 decolourisation efficiency of almost 100% (Figure 4a). As for the MtrC knock out, there was an
225 initial lag in decolourisation which was maintained for the first 24 h, followed by a compensated
226 decolourisation that was more or less the same as that for *Shewanella oneidensis* MR-1 wild
227 type. As a negative control, the dye was added to the media without adding any microbial cells,
228 the results show an average of 8% decolourisation which accounts for the percentage of non-
229 biological degradation.

230 Fig. 4b represents the riboflavin concentration at the end of the MFC system. The figure shows
231 that the highest riboflavin was produced by the MtrC knock out (15.1 μM) and that when the dye
232 was added to the media there was a decrease in riboflavin production (11.9 μM).

233 [Figure 4a&b near here]

234 As for the bioelectricity production, Fig. 5a shows that the MtrC knockout exhibited the highest
235 voltage, this was followed by that obtained when riboflavin was added to *Shewanella oneidensis*
236 MR-1 culture. The figure also shows that the least current was obtained from *Shewanella*
237 *oneidensis* MR-1 culture in the absence of riboflavin. Both voltage and power density followed

238 the same trend for the culture as shown in Figures 5b&c, the highest belonging to MtrC knock
239 out (500 mV) and power density reaching 78 mW/m². The remaining COD was shown to be the
240 least when riboflavin was added to the media (41%), as compared to that without riboflavin
241 (52%) and MtrC knock out culture which showed 46% residual COD (Fig. 5d).

242 In an attempt to assess the decolourisation to be removal or degradation, a UV-visible scan was
243 performed for the samples, the results show that both MtrC knock out culture and riboflavin
244 supplemented cultures (20 and 40 µM) exhibited a complete breakdown of dye as indicated by
245 the complete disappearance of the peak at 480 nm as compared to *Shewanella oneidensis* MR-1
246 without riboflavin which exhibited a decrease in the peak absorbance (Fig. 6).

247 **Analysis of the metabolites produced**

248 The analysis of the metabolites at the end of the MFC system showed no distinctive peaks for
249 both acetic acid and ethanol, on the other hand butyric acid was detected in the media (Table 1).
250 The concentrations were highest for *Shewanella oneidensis* MR-1 (88.9 mg/l) and decreased
251 dramatically when the dye was added. The addition of riboflavin resulted in a slight increase in
252 butyric acid concentrations from 29.7 mg/l for control samples to 32 mg/l for samples
253 supplemented with riboflavin. On the other hand, MtrC knock out produced the lowest butyric
254 acid concentration (9.7 mg/l).

255 **Comparison of dye removal in the presence or absence of MFC**

256 In order to determine if an MFC system is required to achieve better decolourisation, MFC
257 systems were prepared as mentioned in the materials and methods section. The results shown in
258 Figure 7 represent decolourisation in MFC and non-MFC systems in the presence and absence of

259 riboflavin. The results clearly show that it is not the closed MFC system that contributes to
260 decolourisation but the presence of riboflavin in the system.

261 **Toxicity test**

262 To assess the effect of dye on the human Hep G2 cells, we incubated the dye before and after
263 decolourisation with the cells and visualised the live cells using calcein dye. The images shown
264 in Figure 8 show that the fluorescence was minimal when the dye was added before it was
265 treated, on the other hand, the cells incubated with dye after treatment showed fluorescence
266 almost the same as that obtained for control cells.

267

268 **Discussion**

269 *Shewanella oneidensis* MR-1, a classic model exoelectrogen used in bioremediation and
270 electricity production, was used in this study and the effect of added riboflavin as electron shuttle
271 compound was evaluated in terms of azo dye decolourisation and electricity production. The
272 increase in both decolourisation and growth indicates that riboflavin was used by *Shewanella*
273 *oneidensis* MR-1 wild type to transfer the electrons and reduce the azo dye in a matter of hours.
274 The variation of the optimal riboflavin concentration required to achieve high decolourisation
275 and that required to obtain highest current indicates that both decolourisation and electricity
276 production are not necessarily a simultaneous process and that there might be a competition in
277 both functions. There is currently no agreement on the mode of action of bacterial electron
278 transfer. While Chen et al., (2011) and Hsueh et al., (2014) indicated that the two electron
279 transfer processes go in parallel, our results indicate that the process is competitive. Considering
280 that all the mentioned studies used azo dyes as a common chemical structure, this might suggest

281 that the difference could be attributed to the type of organisms used, since they are not the same.
282 Chen et al., (2011) used *Proteus hauseri*, Hsueh et al., 2014 used *Enterobacter cancerogenus*,
283 while in our study we used *Shewanella oneidensis* MR-1 wild type.

284 The electron transport process for azo reduction indicated different inhibition levels when nitrate,
285 copper, azide and ferrous ions were present. The results suggest that inhibition in decolourisation
286 may have occurred as a result of competition for electrons from electron donors. This is in
287 agreement with Hong et al., (2007) who studied the effect of electron donors to understand the
288 mechanism of bacterial anaerobic azo reduction to improve the treatment of azo dye
289 contaminated waste water.

290 'In an attempt to understand the role of direct electron transfer in the azo reduction process,
291 *Shewanella oneidensis* MR-1 was entrapped in alginate beads to preclude the direct contact. The
292 results showed that the decolourisation decreased by almost 3 fold as compared to control cells
293 which were in direct contact with the dye. This result confirms the involvement of both direct
294 and electron mediated decolourisation process. Bacterial electron transport in *Shewanella*
295 *oneidensis* MR-1 involves either direct transfer via outer membrane c-type cytochromes
296 (OMCs), nanowires or indirect electron transfer via endogenously secreted flavins (Yong et al.,
297 2013). Most studies focus on the involvement of membrane bound cytochromes in the electron
298 transfer process (Carmona-Martinez et al., 2011). MtrC is one of the membrane bound
299 cytochromes. Edwards et al., (2015) stated that redox-linked flavin sites in extracellular
300 decaheme proteins are involved in microbe-mineral electron transfer under anaerobic conditions.
301 MtrC combines with flavin mononucleotide to produce flavocytochromes, a semi-reduced flavin
302 that is located at the biofilm-electrode interface (Edwards et al., 2015). From this stand point, an
303 MtrC knock out strain was used to study azo decolourisation and electricity production. The

304 results show that initial decolourisation within the first 24 h was faster in wild types, both with
305 and without riboflavin, the latter being faster. MtrC knock out strain lagged in decolourisation
306 but the rate quickly increased to match that for *Shewanella oneidensis* MR-1 wild type (Figure
307 4a). Results showing residual riboflavin concentrations in the media revealed that riboflavins
308 were endogenously secreted in the media for the MtrC knock out strain. This result suggests that
309 in order for the cells to compensate the lack of MtrC as the end protein in the electron transport
310 chain, the cells resorted to over secretion of Flavin to act as a mediator in the process. The results
311 are the same for both decolourisation and electricity production. While *Geobacter* species were
312 reported to lack the ability to secrete flavins by themselves, *Shewanella oneidensis* MR-1 have
313 been reported to produce quinone-like compounds and flavins which act as electron shuttling
314 compounds (Watanabe et al., 2009). A study focusing on the kinetic measurements of purified
315 OmcA and MtrC revealed that those cytochromes were slower in direct reduction of metal oxides
316 and that this was rapidly increased after the addition of flavins to the medium (Ross et al., 2009).
317 Exploring metabolic pathways can shed light on optimal strategies to maximize the performance
318 of microbial fuel cells (Hsueh et al., 2014). The results obtained indicated that only butyric acid
319 was produced under the employed culture conditions. This suggests the possibility of reusing the
320 butyric acid again by the cells which sustained the electricity production. Identification of
321 metabolites and/or degraded azo dye could shed light on how to increase the decolourisation
322 process in terms of rate and efficiency (Solanki et al., 2013). The debate about MFC Vs. non-
323 MFC in rate and efficiency of decolourisation is still not concluded. Some studies confirm that
324 MFC conditions are required for faster and significant colour removal (Hsueh et al., 2014), while
325 our study indicates that the addition of riboflavin is the key to rapid decolourisation as indicated

326 by the complete disappearance of the dye peak. For a comparison of dye decolourisation rates in
327 MFC and non-MFC conditions, see Fernando (2014).

328 In order to claim that we can re-use the treated coloured wastewater, a toxicity test was
329 performed to assess the quality of the resulting treated water. The results obtained indicate that
330 there is no obvious difference between treated and control cells in viability, as opposed to dead
331 cells resulting from incubation with the dye before treatment. This is a preliminary test that
332 proposes the possibility to reuse. However, more tests are required for confirmation.

333

334 **Conclusion**

335 Deciphering the role of electron shuttling in bioremediation and electricity production reveals
336 information about how to enhance these processes through fine tuning of microbial metabolism.
337 In the current study, there were two main findings; the first results showed that flavin addition
338 plays a role in the decolourisation process which indicates that this process is mediated. The
339 second indicates that electricity production in an MFC does not affect simultaneous dye
340 decolourisation. The study also shows that MtrC was not the responsible protein in both
341 electricity production and decolourisation, confirming that riboflavin is the key player. A
342 question still outstanding is which gene is responsible for decolourisation and which one is
343 responsible for electricity production? We are currently studying the exact role of Mtr pathway
344 genes for both decolourisation and energy production using synthetic biology to answer this
345 question.

346

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351

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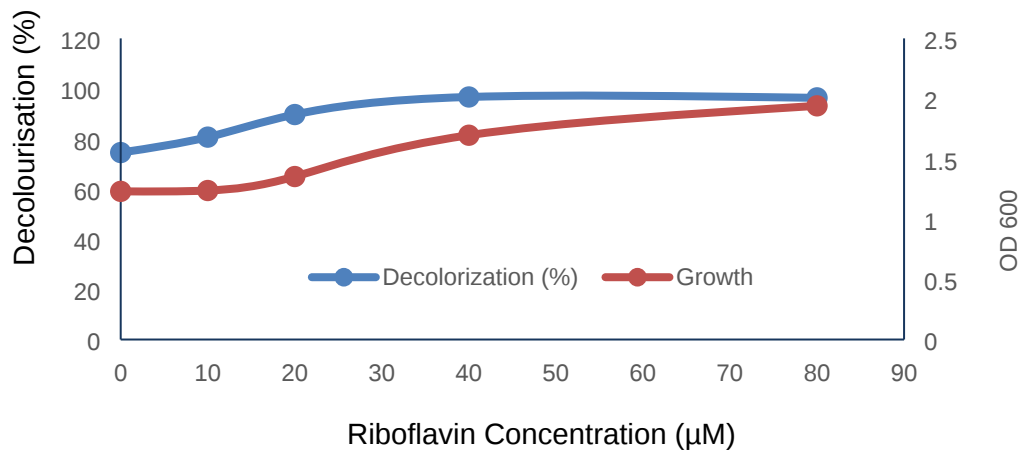
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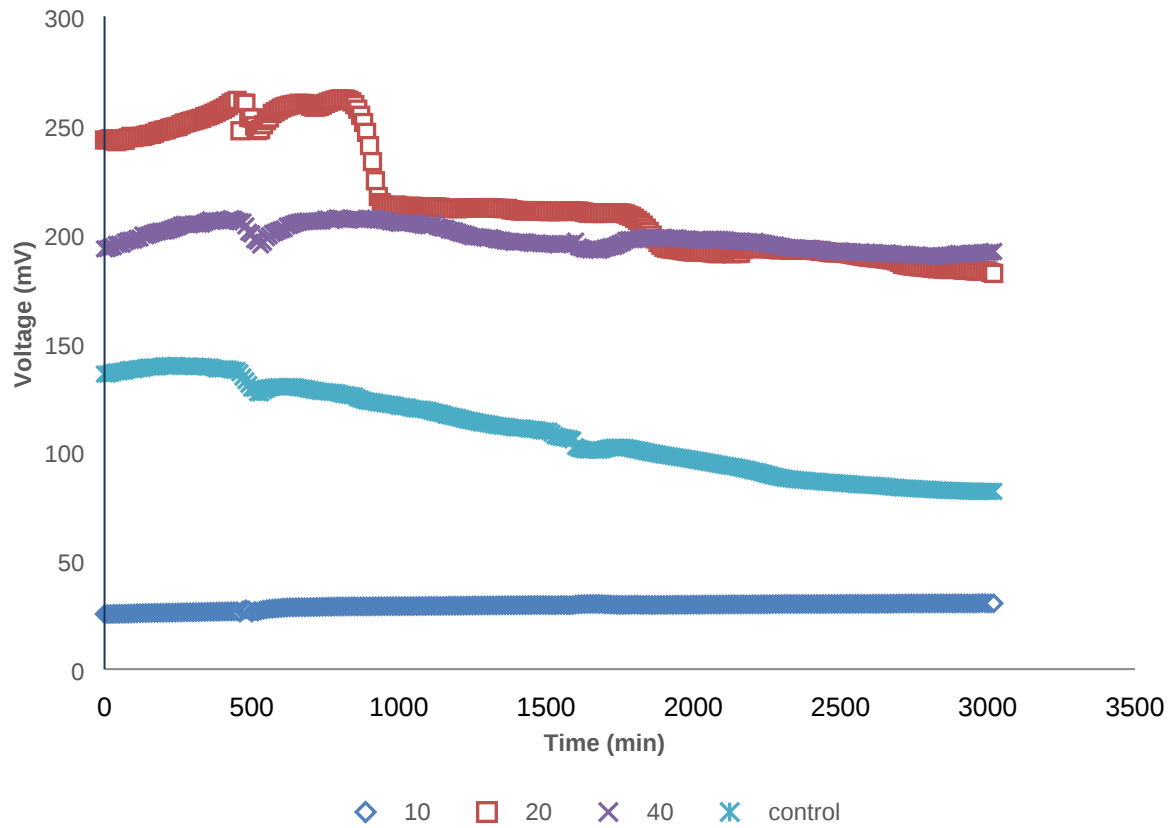
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Figure (1): The effect of riboflavin concentration on the decolourisation of Congo red and growth of *Shewanella oneidensis* MR-1 under non-MFC conditions (anaerobic bottles, results taken after 24 h incubation).



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447 Figure 2(a): Voltage-time profiles for MFCs containing 200 mg/l Congo red and 0, 10, 20, 40

448 μM riboflavin.

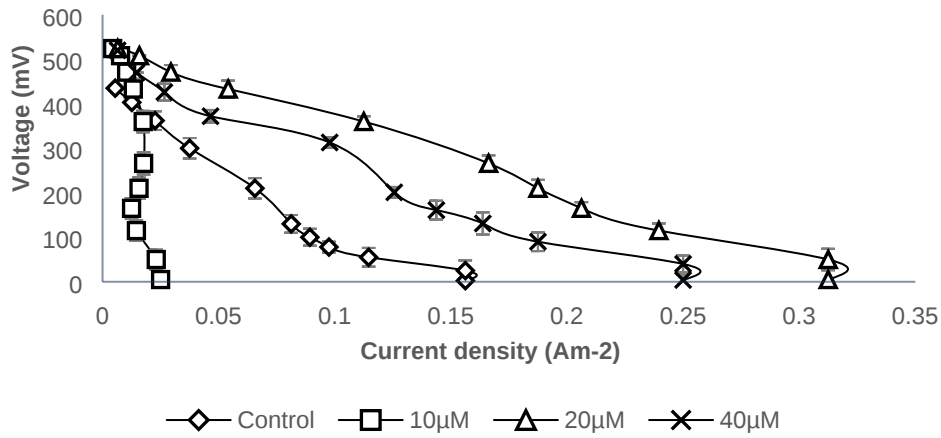
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456 Figure 2(b): Voltage profile for MFCs containing 200 mg/l Congo red and 0, 10, 20, 40 µM

457 riboflavin.

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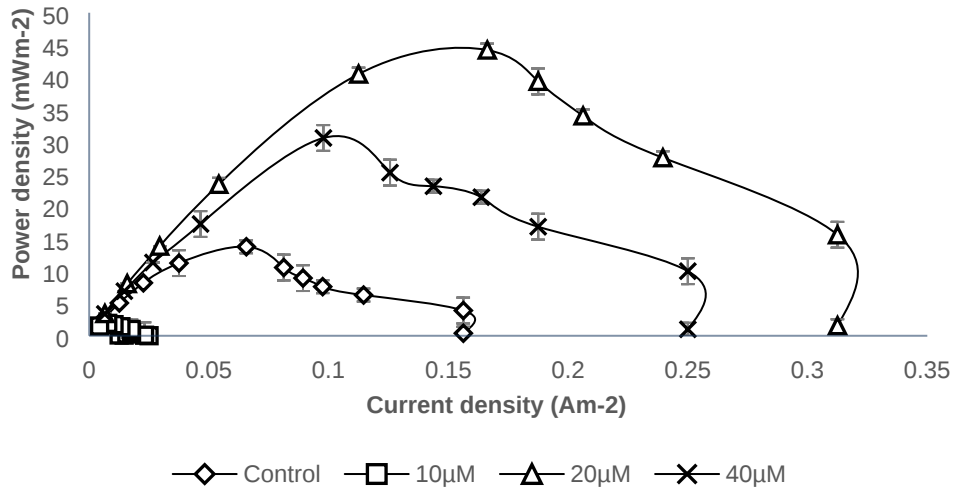
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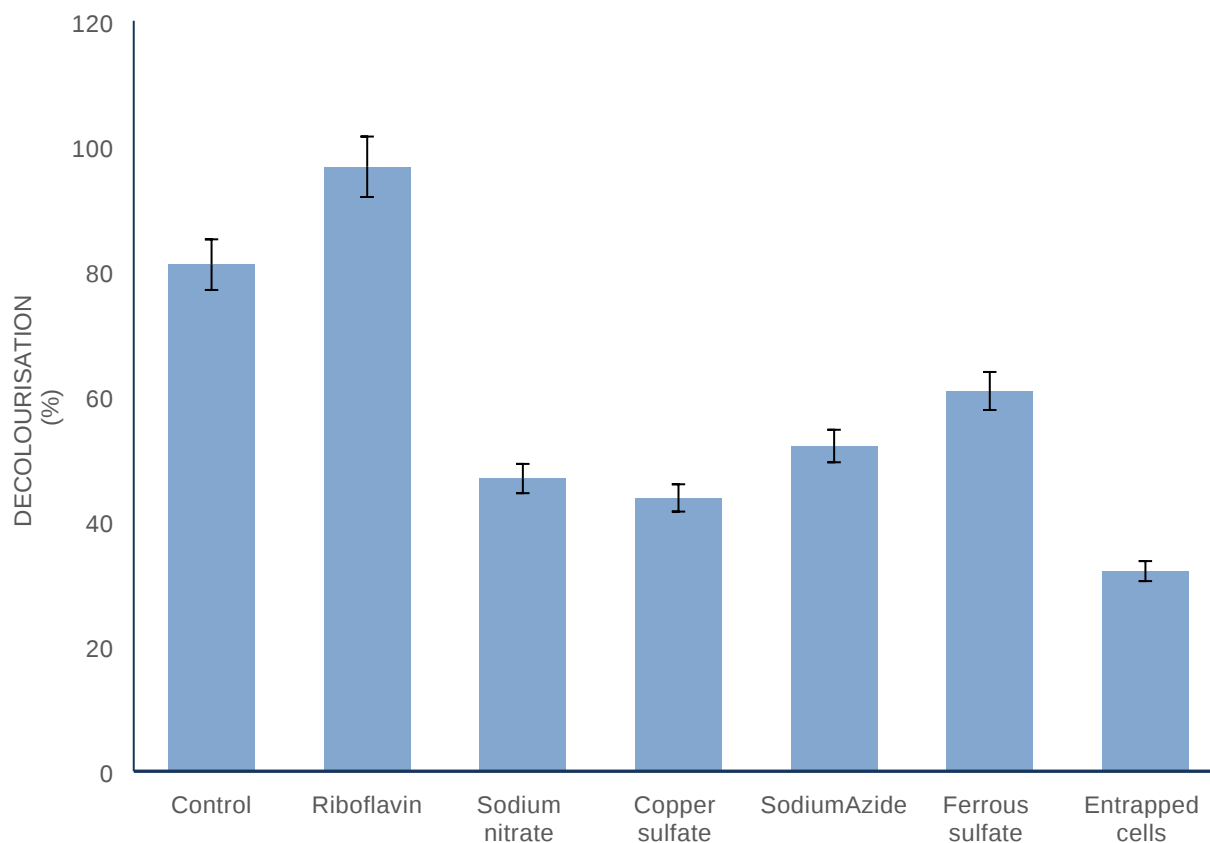
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465 Figure 2(c): Power density profile for MFCs containing 200 mg/l congo red and 0, 10, 20, 40 μM
 466 riboflavin.

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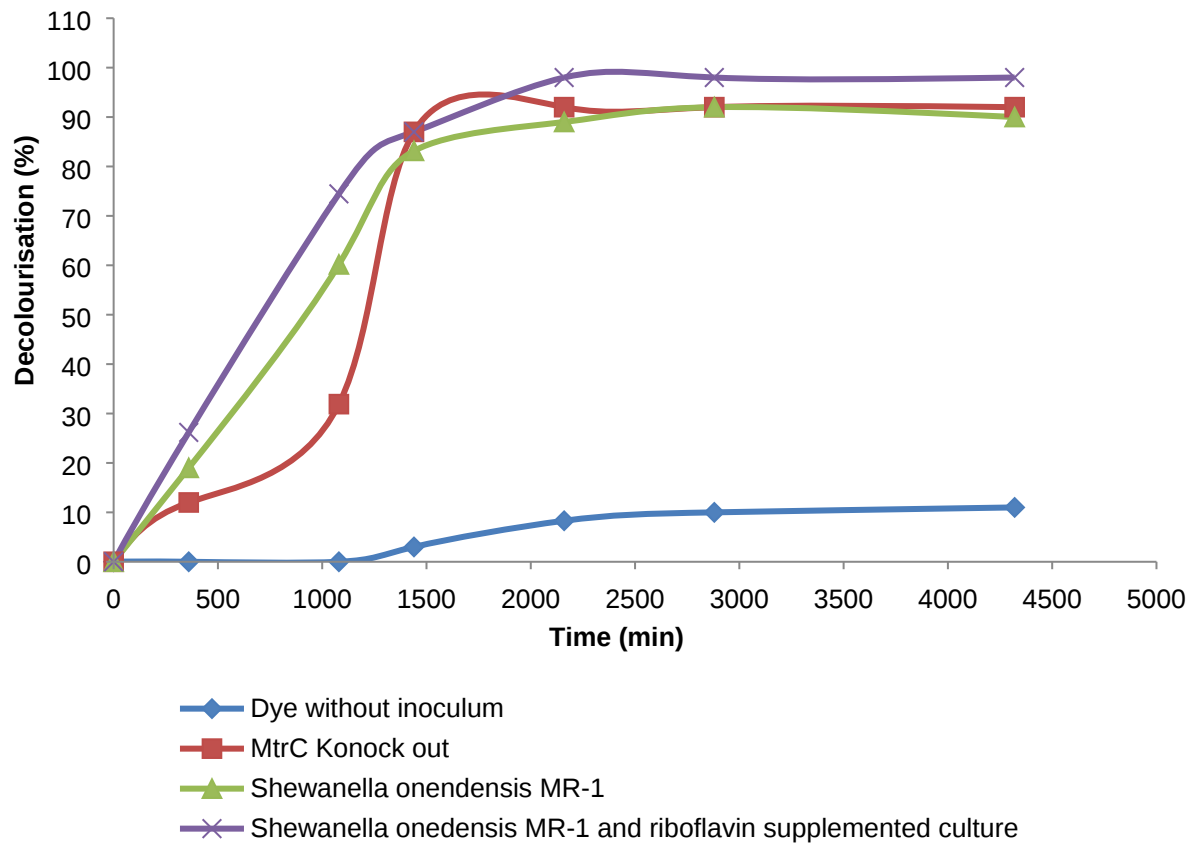
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471 Figure (3): Decolourisation of congo red using *Shewanella oneidensis* MR-1 in non-MFC
 472 conditions (anaerobic bottles) under the following conditions: riboflavin for increasing
 473 decolourisation, sodium nitrate and ferrous sulphate for competitive terminal electron acceptor,
 474 copper sulphate and sodium azide for respiratory inhibition, entrapped cell to prevent direct
 475 electron transfer.

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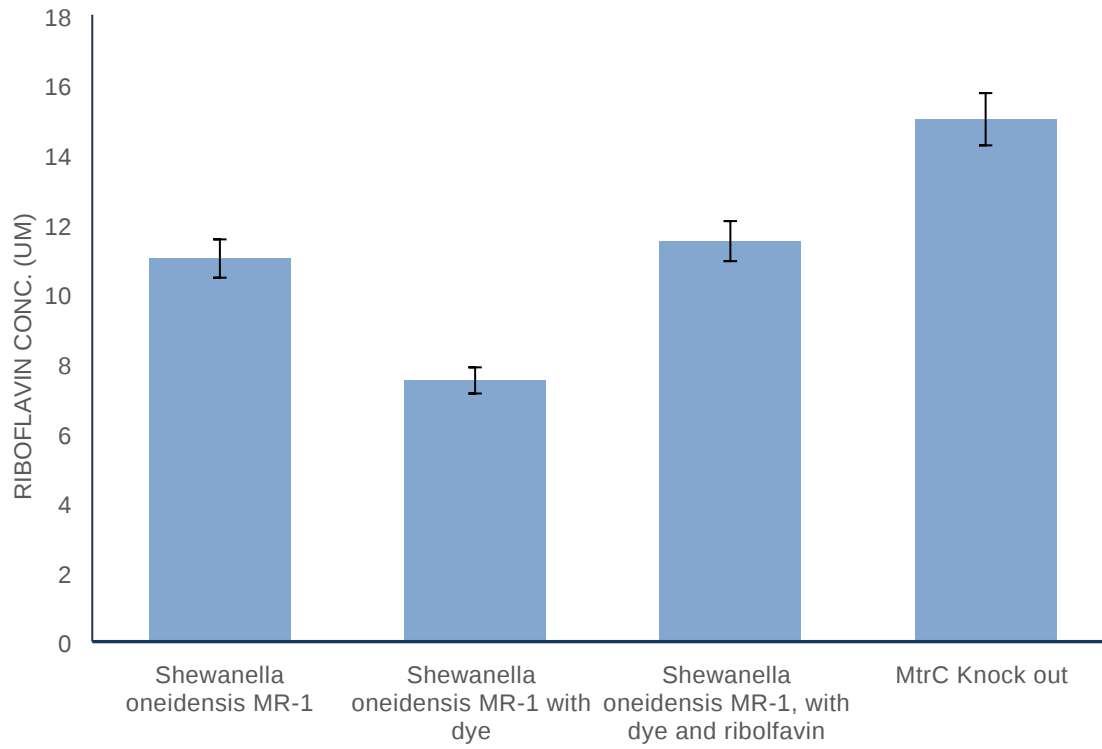
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480 Figure 4(a): Time course of decolorization under MFC conditions for the mentioned cultures.

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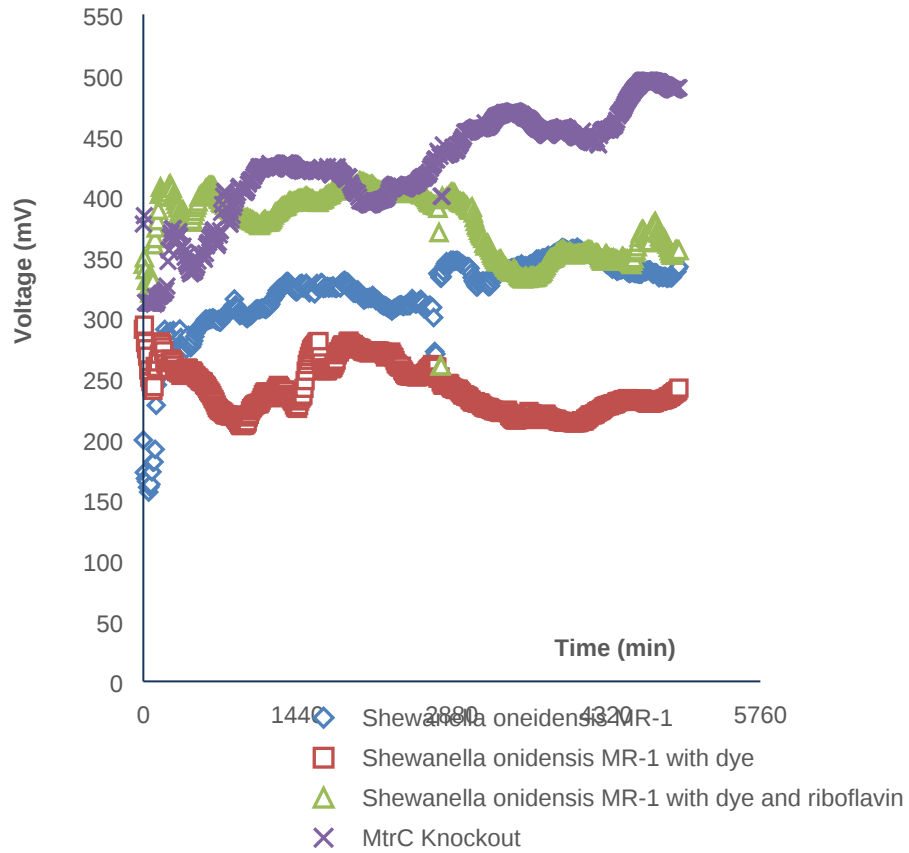
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485 Figure 4(b): The residual riboflavin at the end of MFC process

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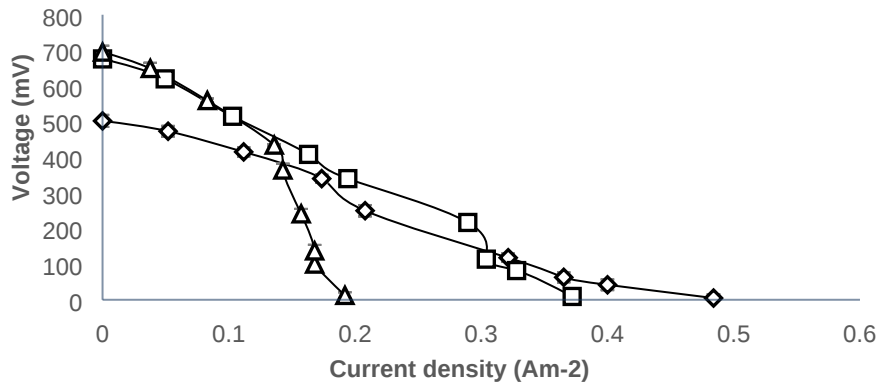
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488 Figure 5(a): Bioelectricity generation profile for MFC containing different culture conditions.

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- ◇— S. oneidensis with MtrC Knockout
- S. oneidensis with Riboflavin and Dye
- △— S. oneidensis with Dye

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493 Figure 5(b): Voltage profile for MFCs under different conditions.

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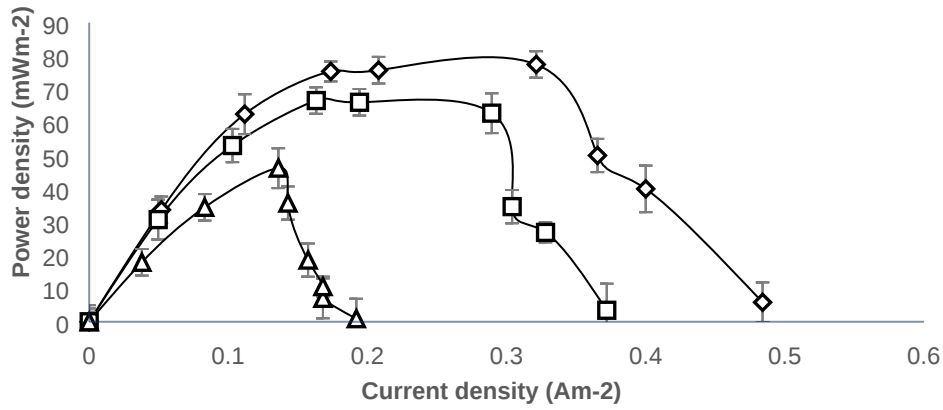
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- ◇— S. oneidensis with MtrC Knockout
- S. oneidensis with Riboflavin and Dye
- △— S. oneidensis with Dye

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501 Figure 5(c): Power density profile under different conditions using 20 uM riboflavin

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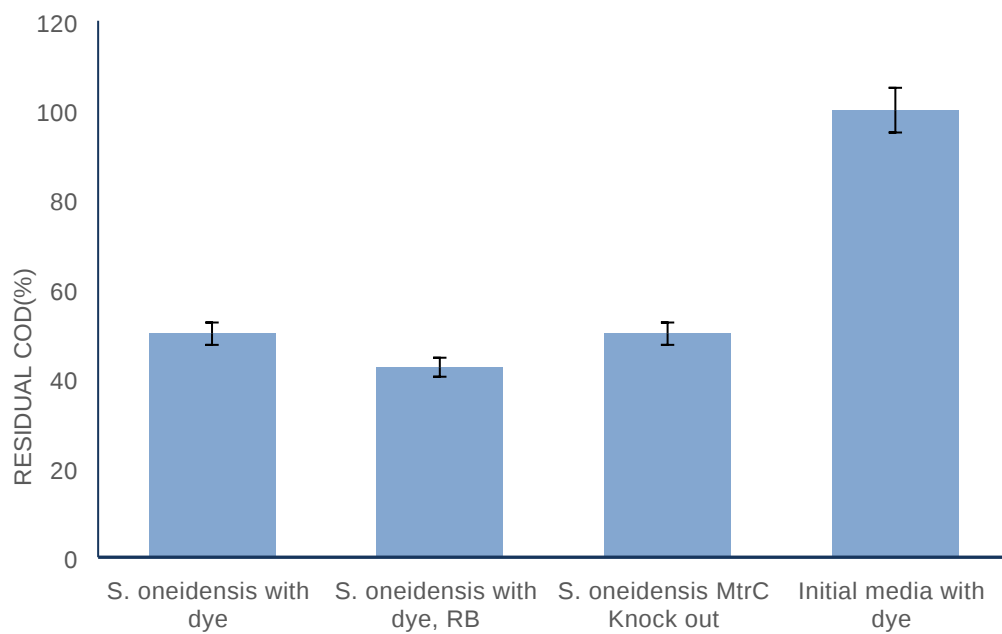
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509 Figure 5(d): Residual COD % for MFC cultures, 20uM riboflavin was added

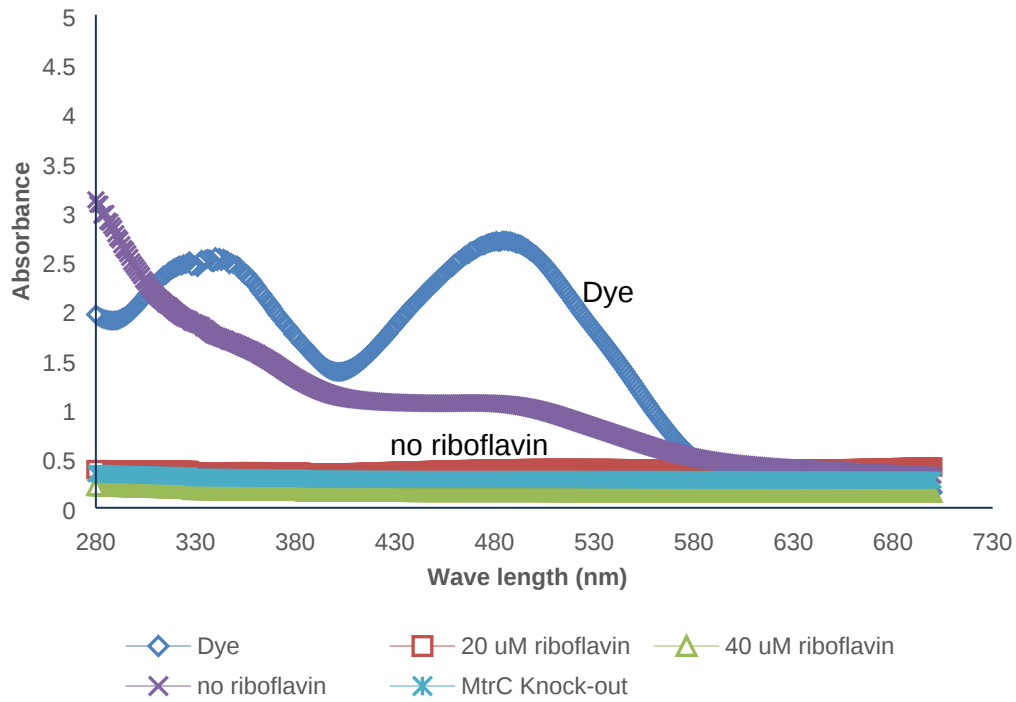
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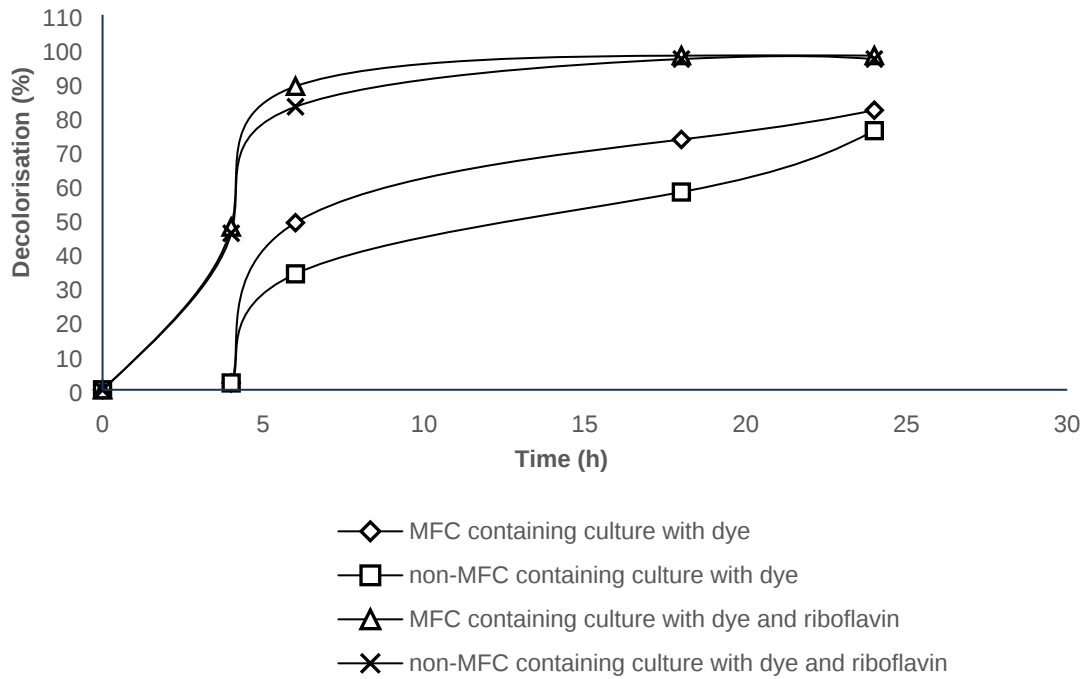


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516 Figure (6): UV-visible spectrum of congo red before and after decolourisation by *Shewanella*
 517 *oniedensis* MR-1 in the absence and presence of riboflavin (20 and 40 uM) and using MtrC
 518 knock out strain.

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522 Figure (7): Decolourisation of Congo red by *Shewanella oneidensis* MR-1 in MFC and non-MFC
 523 conditions and in the presence and absence of riboflavin.

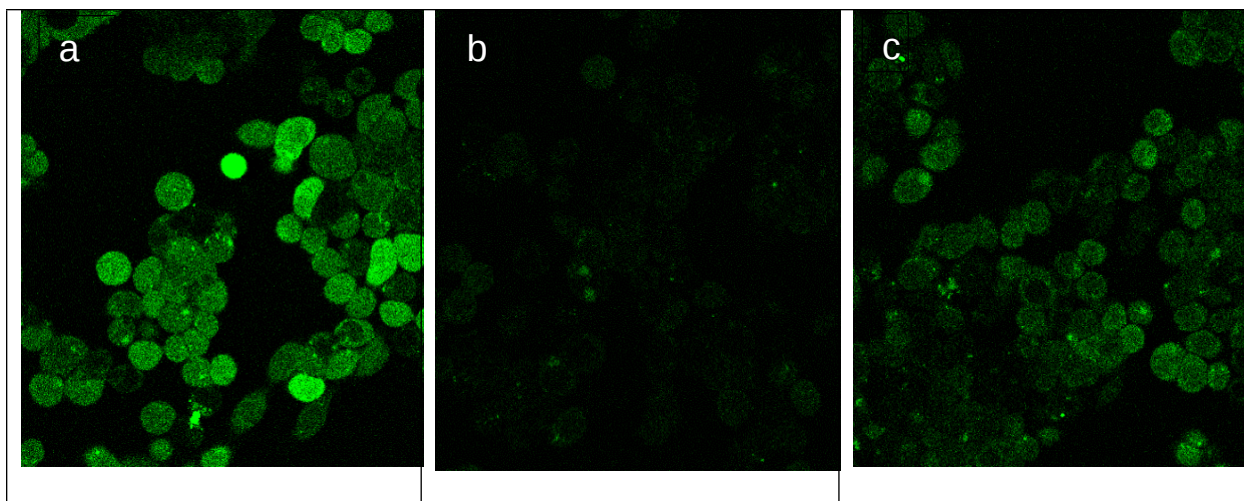
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529 Figure (8): Images of HepG2 cells exposed to different treatments. Images are taken using
530 confocal scanning laser microscopy (CSLM) and represent cells treated with congo red prior to
531 decolorization (b), cells after incubation with treated dye under MFC conditions (c) as compared
532 to control cells grown under regular conditions (a).

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546 Table (1): The metabolites produced at the end of MFC operation

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Test	Fermentation product (mg/ml)		
	Acetic acid	Ethanol	Butyric acid
<i>S. oneidensis</i> MR-1	ND	ND	88.92
<i>S. oneidensis</i> MR-1 with dye	ND	ND	29.692
<i>S. oneidensis</i> MR-1 with dye and riboflavin	ND	ND	32
<i>S. oneidensis</i> MtrC knock out with dye	ND	ND	9.692

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